



Optimizing ethanol and bioelectricity production in sugarcane biorefineries in Brazil



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ABSTRACT

In sugarcane biorefineries, the lignocellulosic portion of the sugarcane biomass (i.e. bagasse and cane trash) can be used as fuel for electricity production and/or feedstock for second generation (2G) ethanol. This study presents a techno-economic analysis of upgraded sugarcane biorefineries in Brazil, aiming at utilizing surplus bagasse and cane trash for electricity and/or ethanol production. The study investigates the trade-off on sugarcane biomass use for energy production: bioelectricity versus 2G ethanol production. The BeWhere mixed integer and spatially explicit model is used for evaluating the choice of technological options. Different scenarios are developed to find the optimal utilization of sugarcane biomass. The study finds that energy prices, type of electricity substituted, biofuel support and carbon tax, investment costs, and conversion efficiencies are the major factors influencing the technological choice. At the existing market and technological conditions applied in the upgraded biorefineries, 300 PJ y⁻¹ 2G ethanol could be optimally produced and exported to the EU, which corresponds to 2.5% of total transport fuel demand in the EU. This study provides a methodological framework on how to optimize the alternative use of agricultural residues and industrial co-products for energy production in agro-industries considering biomass supply chains, the pattern of domestic energy demand, and biofuel trade.

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1. Introduction

Sugarcane is one of the key renewable sources in Brazil. In 2013, it comprised 19% of the country's energy matrix [1]. Sugarcane juice, bagasse (stalk fibers: fibrous residue left over after squeezing sugarcane for its juice), and sugarcane leaves/tops (straw, also known as trash) each represents one-third of sugarcane energy content [2,3]. 40% of the fuel used in Otto-cycle engines (light duty vehicles) comes from first generation sugarcane juice ethanol in Brazil [3,4]. However, the lignocellulosic portion of the sugarcane biomass, which includes bagasse and trash, is still underutilized [5–11]. Surplus bagasse obtained in sugarcane mills and trash left or burnt in the field during harvesting can also be collected and

used for energy production. Bagasse and trash can be alternatively used as fuel for power (electricity) generation or feedstock for second generation biofuel.

There is room for upgrading the existing sugarcane mills as there is plenty of surplus sugarcane biomass (i.e. cane trash and bagasse) readily available. Cane trash and bagasse also have similar fuel characteristics, making them suitable for energy production [12]. There are several biomass conversion technologies, for that purpose, for example, cogeneration systems, thermochemical, and biochemical processes [13–17]. In this context, it is important to analyze alternatives and determine the best suitable option for optimally producing energy services and diversifying the industry. Both techno-economic and environmental performance need to be considered. A concept of 'biorefinery', which is analogous to the 'oil-refinery', is currently being developed for the conversion of lignocellulosic biomass, and simultaneous production of commercial liquid biofuels, heat and power, and a wide range of bio-products [18,19]. The utilization of lignocellulosic biomass feedstock (e.g. crop harvest residues: straw/trash and industrial co-products: bagasse) for biofuel production would be preferable

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considering the potential impacts of sugar/starch and oil seeds based biofuel production on food security and land use changes [16,20]. Biomass based advanced cogeneration technologies for electricity generation are quite mature and commercially available [21,22] while second generation biofuel from lignocellulosic biomass has not yet become an industrial reality due to high investment and production costs [16,23]. Meanwhile, the soaring biofuels demand, especially due to renewable mandates and targets in many countries, is promoting global market formation and trade of biofuels [24]. Therefore, domestic demand, international biofuels market/trade, and the competition with electricity generation from the use of lignocellulosic biomass should be taken into account while selecting the suitable biofuel/bioenergy pathways. This study considers the sugarcane mills operating in one of the sugarcane producing states in Brazil, and their upgrading into biorefineries for producing bioelectricity and/or second generation (2G) ethanol using sugarcane biomass. Sugarcane bagasse and leaves/trash can be used in the production of bio-products [25] but the utilization of sugarcane biomass for non-energy production is beyond the scope of this paper. The study investigates the best technological options - second generation (2G) ethanol (2G option) or bioelectricity (electricity option) - for converting sugarcane biomass to useful energy products.

A number of studies have performed the techno-economic analysis of biofuel production at the plant level [6,7,9,11,26–28]. Seabra et al. (2010) have evaluated the techno-economic performance of thermochemical and biochemical conversion of sugarcane residues, considering sugarcane mill clustering [26]. Walter and Ensinas (2010) have described the technological pathways of biofuel production from sugarcane biomass and analyzed the impact of process integration with a conventional sugarcane distillery [7]. Systems performance is simulated for the technical, economic and environmental merit of power generation and ethanol production from sugarcane residual biomass, considering conversion plants adjacent to a sugarcane mill [6]. Dias et al. (2011) have performed simulation studies to determine the suitable option when selecting second generation or bioelectricity from the sugarcane biomass feedstock [9]. Macrelli et al. (2012) have described the competitiveness of second generation ethanol from sugarcane bagasse and leaves [10]. Lago et al. (2012) have demonstrated the positive conditions for the development of second generation ethanol derived from sugarcane biomass (bagasse and cane trash) in Brazil considering different industrial scenarios [29]. Dias et al. (2012) have examined how process optimization increases the production of second generation ethanol in sugarcane distilleries [11]. Recently, Furlan et al. (2013) and Dias et al. (2013) have investigated the economic advantages of a flexible (able to switch between 2G ethanol and bioelectricity production) sugarcane biorefinery [30,31]. Some authors claim that lignocellulosic ethanol may require policy support for implementation [32]. In addition, Dias et al. (2012) have simulated stand-alone and integrated second generation ethanol production from sugarcane biomass considering different technological scenarios [28]. Tittmann et al. (2010) have presented a spatially explicit techno-economic optimization model of bioenergy and biofuels production system in California, considering location/size of bioenergy plants, conversion technologies, and feedstock profile and its supply chain configuration [33]. The model aims at maximizing the profit of a biofuel industry at given feedstock price, transportation cost, conversion cost, and price for fuels, electricity, and co-products. However, no analysis has been carried out at the regional level yet, considering the entire biofuels production chain in general and the sugarcane biofuel (1G ethanol and 2G ethanol) production chain in particular. In addition, previous studies have not addressed the climate impacts or GHG offsets of the biofuel

production systems. In addition to exploring optimal technological options, this study also presents the dynamics of the total costs and lifecycle emissions by internalizing the costs of emissions in the optimization model.

This study performs a techno-economic analysis for the bulk of sugarcane production area and industries located in the Brazilian state of Sao Paulo (SP). Biofuel production and international trade have been gradually growing over the last decade [34]. Therefore, it is important to understand how policies and economic/market factors/forces (e.g. price, carbon tax, biofuel support, etc.) affect the international trade of liquid biofuels. The trade of 2G ethanol to the European Union (EU) is taken into account here. The study considers that ethanol produced from sugarcane juice (1G ethanol) through fermentation is domestically consumed while the second generation (2G) ethanol, if produced, can be exported to the EU. Bioelectricity produced is fed into the grid and utilized in Brazil. 1G ethanol is already mature and commercially competitive. However, 2G ethanol is still not produced in commercial scale. Therefore, we scrutinize the technological choices and the role of market and policy instruments for energy (2G ethanol and/or bioelectricity) production from sugarcane biomass, also looking into international trade of 2G ethanol.

The study examines the alternative uses of sugarcane biomass (i.e. bagasse and cane trash) for 2G ethanol and/or bioelectricity production in the state of Sao Paulo in Brazil. The study performs the techno-economic optimization analysis of sugarcane mills, assuming technological improvements of existing mills. There is still a limited amount of research in modeling of biomass supply chains when it comes to investigating the impact of technological change, policy drivers/incentives, and market volatilities [35]. The study considers how the energy prices, conversion costs, and policy instruments such as biofuel support and carbon tax affect the choice of technology (2G ethanol option or electricity option), including the export of bioethanol to the EU. This paper aims to complement existing research studies, which are mainly focused on optimization of the economic and environmental benefits of biorefineries at the plant level in Brazil and other countries, by examining the costs and emissions of the entire supply chains, as well as the interactions with external parameters (e.g. energy prices, biofuel support, carbon tax, and international biofuel trade) in providing sustainable energy services for the welfare of the region.

The BeWhere model is used to determine the choice of technological improvements. The model is spatially explicit and has previously been applied for assessing the optimization of bioenergy production, mainly aiming at identifying the optimal location and size of biomass conversion units in Europe, see Refs. [36–39]. Sugarcane biomass is a geographically dependent renewable resource. It is important to develop an optimization model for determining suitable size/location of biofuel plants and conversion technologies, considering biomass supply, transport costs, and energy demand/prices. As the location and size of sugarcane mills is fixed in this study, we only simulate the technological options using the sugarcane biomass (bagasse and trash). This spatially explicit study is the first study of its kind in the Brazilian context in which sugarcane biomass - agricultural residue (tops/leaves or trash) and agro-industrial co-product (bagasse) - is used for energy production in sugarcane biorefineries. The study also provides important information on lifecycle emissions and costs/prices of advanced biorefineries using lignocellulosic sugarcane biomass in Brazil. It shall contribute for further development of the BeWhere model when the country seeks alternative pathways for producing modern bioenergy services, considering all features of the spatial modeling approach. Many developing countries have a huge potential to harness bioenergy/biofuel derived from crop residues (e.g. sugarcane trash, rice husk, straw, etc.) [40–42]. This model

could be useful for identifying the optimum utilization of residual biomass or crop residues in these developing countries in terms of suitable technological options (e.g. conversion into 2G advanced biofuel or efficient cogeneration technologies), size/location of biofuel plants, policy instruments (incentive or biofuel support), costs/prices, and market factors.

The study is organized in five sections. Following this introduction, sugarcane mills, bioenergy systems, and upgraded technological options are described in Section 2. Section 3 presents the methodology and research approach adopted, indicating data sources and model inputs used in the simulation. The estimation of systems costs and lifecycle GHG emissions are also carried out. Results and discussion are presented in Section 4. Finally, concluding remarks are made in Section 5 with an emphasis on the main policy implications of the study.

2. Sugarcane mills and bioenergy systems

Sugarcane mills are being converted into biorefineries to produce more energy products and services. In Brazil, approximately

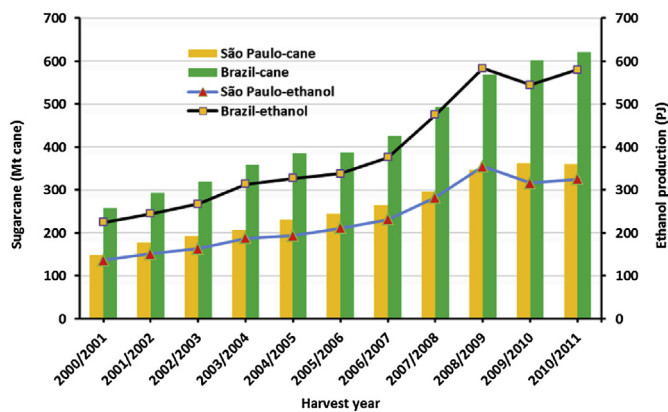


Fig. 1. Trend of sugarcane and ethanol production in Sao Paulo state and Brazil [4]. Note: primary and secondary y-axis represent the total sugarcane production (million tonnes or Mt) and ethanol production in Peta Joule (PJ) respectively; 1 PJ is equal to 47.2 million liters.

Table 1

Characteristics of sugarcane biorefineries considered in this study.

Parameters	Values ^d	Technological options		
		Conventional technology	Upgraded	
			Electricity option	2G option
Process capacity ^a	2 Mt cane per year	x	x	x
Juice ethanol yield	91 L/t cane	x	x	x
Conventional cogeneration plant	22 bar/300 °C	x	–	–
Efficient cogeneration plant ^b	90 bar/520 °C	–	x	x
Bagasse availability	280 kg/t cane (50% moisture content)	x	x	x
Unburned harvesting	100%	x	x	x
Total trash yield	280 kg/t cane (50% moisture content)	x	x	x
Trash availability ^c	70 kg _{dry} /t cane (50% collection)	–	x	x
Sugarcane biomass (bagasse and trash) available for electricity and/or 2G ethanol production	65%	–	x	x
Surplus electricity generation	150 kWh/t cane	–	x	–
Second generation ethanol production	41 L/t cane (i.e. 300 L/t dry cane biomass)	–	–	x
Project year	25 years	x	x	x
Interest rate	10%	x	x	x

^a This capacity is also used as the base for analyzing costs, see Section 3.1 and [9].

^b It is considered that 2G ethanol option also uses efficient cogeneration plant, but for providing heat and power to the refinery. Surplus biomass is used for the production of ethanol.

^c 50% trash is only available for upgraded technologies.

^d Sources: Juice ethanol yield [6], Surplus sugarcane biomass (authors' estimation based on efficient cogeneration (CHP) plant), surplus electricity generation [21], Second generation ethanol production [43].

40% of the sugarcane produced in the harvest years 2008/09 and 2009/10 was used to produce sugar and the rest was used for ethanol production. The state of Sao Paulo (SP) alone produces 60% of all sugarcane in Brazil [4], see Fig. 1. In this study, we assume that all existing sugarcane mills in the state SP are transformed into biorefineries focused on energy products. This means that sugar demand would have to be met by other sugarcane producing states in Brazil.

After harvesting, sugarcane is crushed to extract the juice. The juice is used to produce first generation (1G) ethanol. Bagasse is the fibrous residue left after extraction of the juice and it is combusted in a boiler, for production of heat and electricity. The average bagasse availability in Brazil is 28% (at 50% moisture content) of the sugarcane production. During sugarcane harvesting, abundant sugarcane trash/waste (i.e. tops, leaves) is left in the fields, which can also be used as fuel in cogeneration plants. Trash yield is 280 kg (50% moisture) per tonne of cane stalk. 50% of the cane trash is left in the field to maintain soil quality [5]. Therefore, 50% trash is available for bioenergy conversion, considering the elimination of burning practices in the state of Sao Paulo (see Table 1). It should be mentioned that the optimal amount of cane trash to be left in the sugarcane field, considering both economic and environmental benefits of using it has not been investigated yet [3].

2.1. Sugarcane bioenergy systems: the choice of technology

The study includes three technologies: one conventional technology and two upgraded technologies, viz., efficient cogeneration systems for electricity generation (electricity option) and second generation (2G) ethanol through biochemical conversion of sugarcane biomass (2G ethanol option), (Fig. 2). Table 1 shows the key parameters and characteristics of the biorefineries considered in this study, while Table 2 presents the conversion efficiencies in the three technological options simulated.

The upgraded technologies use the surplus sugarcane biomass (bagasse and trash) for the generation of 2G ethanol and/or bioelectricity, in addition to the production of 1G ethanol from sugarcane juice. It is important to note that approximately 65% of the sugarcane biomass (i.e. bagasse and trash) is available for conversion to bioelectricity or 2G ethanol in the upgraded options

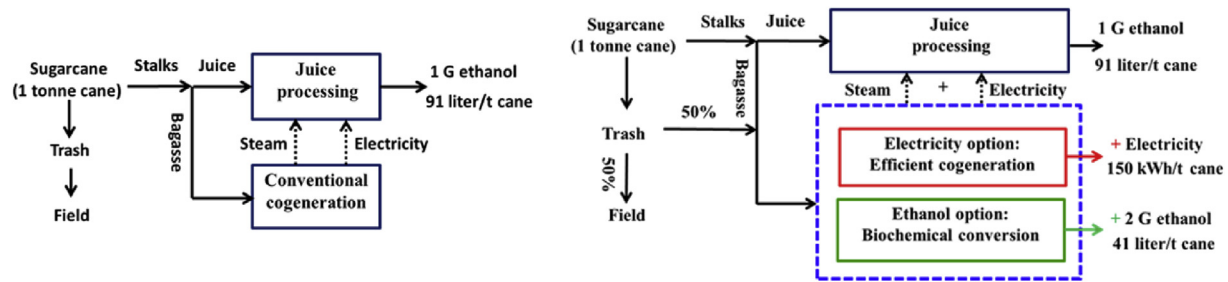


Fig. 2. Technological options: Conventional technology (left) and Upgraded technologies (right).

Table 2

Conversion efficiencies of biorefineries (PJ/Mt cane).

Energy products	Technological options		
	Conventional technology	Upgraded	
		Electricity option	2G ethanol option
Juice or 1G ethanol	1.929	1.929	1.929
Electricity	–	0.540	–
2G ethanol	–	–	0.868
Total energy (PJ/Mt cane)	1.929	2.469	2.797

Notes: juice ethanol yield: 91 L/t cane, 2G ethanol yield: 41 L/t cane, electricity generation: 150 kWh/t cane (see Table 1 for references).

Electricity required for processing (in sugarcane biorefineries) is not considered. A small amount of surplus electricity in conventional technology, which ranges from 0.036 to 0.09 PJ/Mt cane (i.e. 10–25 kWh/t cane, is also neglected).

(see Table 1). Bioelectricity can be sold to the grid while 2G ethanol can be exported to the EU to meet the biofuel target in the transport sector or used in Brazil if exports do not have benefits.

2.1.1. Business as usual/conventional technology

The business as usual or conventional technology only produces ethanol from sugarcane juice and bagasse is combusted to generate heat and power required for the sugarcane mills using back-pressure steam turbine cogeneration systems at low levels of pressure and temperature (~22 bar/300 °C) [3,44]. The conventional sugarcane mills are self-sufficient in their internal energy requirements using bagasse as a fuel in boilers with a little or no electricity sold to the grid [3,6]. It is assumed that there is no surplus bagasse or electricity in the conventional mills as the sugarcane mills are traditionally designed to meet the internal energy requirements. Generation of a small amount of surplus electricity (i.e. 10–25 kWh/t cane) in the conventional sugarcane mills [6] is neglected.

2.1.2. Upgraded technology: electricity option

In sugarcane industries, cogeneration plants are being upgraded to produce surplus electricity in Brazil. Cogeneration (i.e. condensing-cum-extraction steam turbine) with high pressure boilers and turbines (up to 105 bars and 525 °C) are mature and commercially available, and can produce 150 kWh/t cane of surplus electricity, utilizing excess bagasse and trash/residues [21]. The surplus electricity is connected to the grid. It should be pointed out that bioelectricity is mainly produced in the dry season, complementing the electricity from hydropower, and thereby reducing the use of fossil based power generation at the margin.

2.1.3. Upgraded technology: 2G ethanol option

Sugarcane biomass (bagasse and trash) basically contains cellulose, hemicellulose and lignin. Thus it can be converted into fermentable sugars and then biofuel. At present, conversion of lignocellulosic materials (e.g. agricultural residue: cane trash, and agro-industrial co-product or residue: bagasse) to ethanol is not

commercially available and still in the phase of development. Several studies have been done, investigating different conversion processes and their techno-economic performance [6,7,9–11,26]. In this study, the biochemical conversion of sugarcane biomass is used. Fig. 3 shows the structure of upgraded sugarcane biorefinery, including the 2G ethanol conversion processes. The process consists of steam explosion pretreatment of biomass, followed by the enzymatic hydrolysis, fermentation and distillation. Solid residues (i.e. lignin) are used as fuel in the boiler. Pentose-rich stream is bio-digested to produce boiler fuel: biogas. Surplus heat and electricity are not considered in this route.

3. Methodological approach and data sources

3.1. Methodology

Biofuel models and optimization tools can be used to address the sustainability issues associated with biofuel supply chains in terms of environment, society, and economy [45]. In this study, a mixed integer linear program (MILP) [46], BeWhere, is used to optimize the choice of technology for producing energy products and services in sugarcane biorefineries. A detailed description of the model can be found in the previous literature [47,48]. The model has been used in several optimization studies for bioenergy production, especially from forest and wood residues in the EU [37,38,49]. Fig. 4 provides a schematic sketch of the model as applied in this study on energy production from agricultural feedstock in Brazil. The model is spatially explicit and minimizes the costs of the entire biofuel supply chain of sugarcane bioenergy systems, including sugarcane production (agricultural practices), feedstock transportation, biomass processing, and biofuel transportation. The costs for emitting GHG emissions, i.e. carbon tax, are also considered. It should be noted that the BeWhere model is robust and it has been used in a number of spatially explicit optimization studies in making decisions on the choice of technological options for energy production from the same lignocellulosic feedstock. For example, the selection on combined heat and power

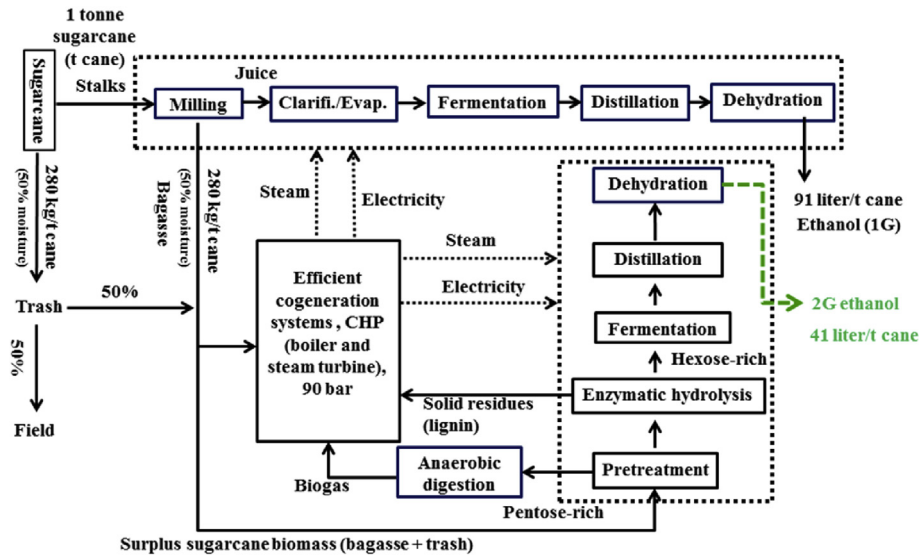


Fig. 3. Biochemical conversion of sugarcane biomass into ethanol – a schematic diagram.

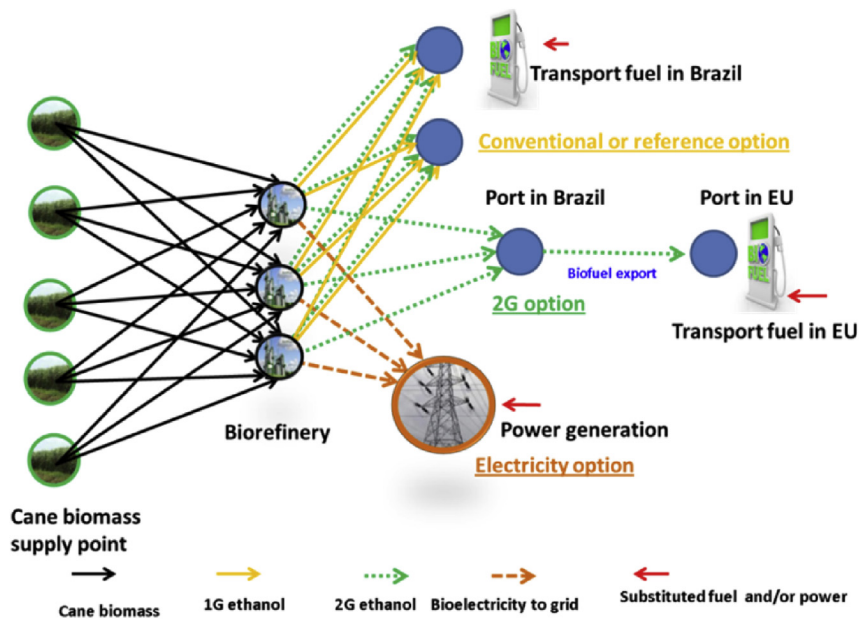


Fig. 4. A schematic diagram of the BeWhere model for sugarcane biorefinery in Brazil. Note: Biomass and energy flows are shown by arrow marks. Red arrow shows the additional fossil fuel needed to meet the demand. (For interpretation of the references to colour in this figure legend, the reader is referred to the web version of this article.)

(CHP) or second generation biofuel production in Europe [39,49] and technology mix (methanol and CHP) of bioenergy production in Finland [38] were identified, considering the costs of the whole supply chain and different policy scenarios (e.g. carbon cost and biofuel support).

The model considers the processing of sugarcane feedstock (stalks and trash/residues) for energy services in the state of Sao Paulo (SP). The study region is divided into grid cells with a 0.1° spatial resolution (approx. 10 × 10 km). All sugarcane mills that fall under a single grid cell are considered together as one, resulting in a total of 158 sugarcane biorefineries in the whole state. As mentioned earlier, the study considers that ethanol produced from sugarcane juice (1G ethanol) through fermentation is domestically consumed in Brazil. This analysis finds the most optimal pathways in the conversion of sugarcane biomass into the second generation

(2G) ethanol and/or bioelectricity using the available surplus bagasse in sugarcane mills and residual biomass (tops/leaves or trash) collected from the sugarcane field. The second generation (2G) ethanol, if produced, can be either consumed in Brazil or exported to the EU depending on market and technological parameters. Bioelectricity produced is fed into the grid and utilized in Brazil. The model does not consider the dynamics of the sugarcane expansion and new sugarcane biorefineries, but incorporates existing sugarcane mills that would be upgraded for increased production of energy services, utilizing excess bagasse and trash/residues. The size and location of the existing sugarcane mills are obtained from two different sources, UNICA [4] and Sugarcane Technology Center [50], respectively. Fig. 5 shows the size and location of the sugarcane mills. Distances between all the grid points of the existing sugarcane mills are computed using the GIS

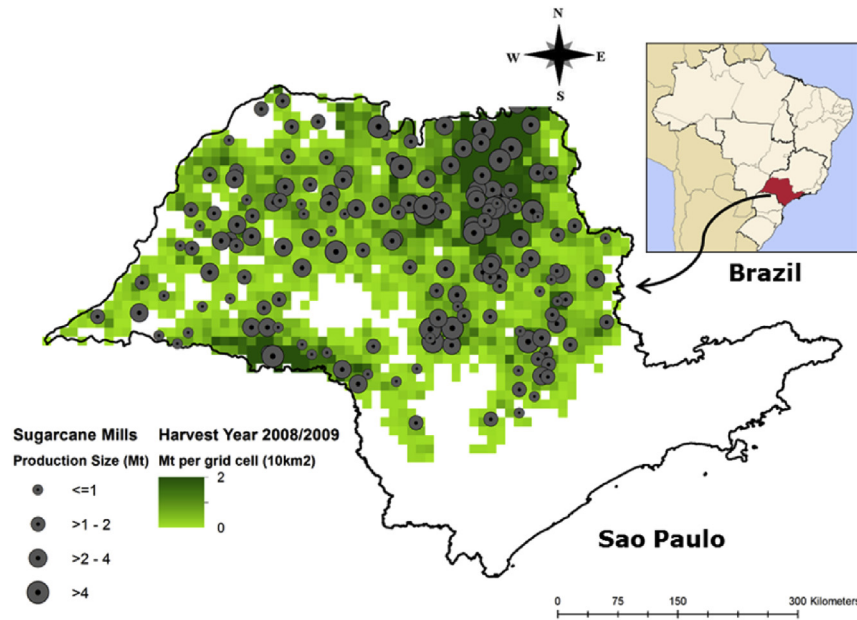


Fig. 5. Size and location of existing sugarcane mills in the state of Sao Paulo (SP), Authors' projection using data from Refs. [4,50].

software. The distance is used for estimating costs and emissions related to transport of sugarcane feedstock between sugarcane fields and plants.

The objective function is to minimize the total cost (C_{total}) in the supply chain, which is expressed as

$$C_{total} = C_{supplychain} + E_{supplychain} \cdot C_{CO_2eq} \quad (1)$$

where $C_{supplychain}$ is the supply chain cost, $E_{supplychain}$ is the supply chain emissions, and C_{CO_2eq} is the cost for emitting GHG emissions.

The supply chain cost ($C_{supplychain}$) consists of: feedstock (sugarcane and trash) cost and transportation cost (to the production plant), investment and production costs, biofuel transport cost to specified supply points, fossil fuel (i.e. gasoline) cost for transport, and income from the sale of bioelectricity. Note that biofuel is transported to gas stations within the state of Sao Paulo (SP) and/or to the port (Rotterdam/the Netherlands) in the EU via the port of Santos located in the state of SP. The cost of gasoline in Brazil and in the EU is different.

The supply chain emissions ($E_{supplychain}$) include: Emissions from sugarcane production/agriculture practices, emissions from sugarcane/trash transport, emissions from plant operations,

emissions from biofuel transport, and avoided emissions from substituted fossil based transport fuel (in Brazil and the EU) and fossil based electricity. In the optimization model, carbon tax is applied to the GHG emissions (CO_{2eq}) associated with production chains of advanced conversion technologies, viz. electricity option (efficient cogeneration) and 2G ethanol option (biochemical conversion of sugarcane biomass), including emissions savings from potential substitutions of fossil based electricity or transport fuel.

The total cost is minimized subject to a number of constraints related to feedstock supply, operation balance in production plants, biofuel trade, and energy demand, see Refs. [47,48] for the mathematical expression on how to formulate the objective function and constraints. The model inputs are: feedstock availability, size and location of the existing plants, transportation distance, annualized costs, emission factors, carbon tax, plant efficiencies, and prices of fuel and power. The model solves the problem by selecting the least costly technological option, considering the whole supply chain cost, emissions, and prices. Thus it does not optimize the profit of a single biorefinery, but rather considers the entire system for the welfare of the region. The resulting model output includes: the choice of technological option, supply chain costs and emissions, the share of 2G ethanol and bioelectricity, and amount of biofuel

Table 3
Investment costs of sugarcane biorefinery (MUS\$).

Components	Technological options ^a		
	Conventional technology ^b	Upgraded	
		Electricity option	2G ethanol option
Juice extraction	22.5	22.5	22.5
Juice treatment, fermentation and distillation and dehydration ^c	35.7	35.7	35.7
Cogeneration	45.0	83.7	51.9
Automation, buildings etc.	57.0	57.0	74.0
2G ethanol conversion ^d	—	—	102.0
Total investment (MUS\$)	160.2	198.9	286.1

^a Processing capacity considered is 2 Mt cane per year.

^b Costs are adopted from Ref. [9] and a scaling factor 0.7 is used, when necessary.

^c Molecular sieves for ethanol dehydration is used.

^d Investment costs for 2G ethanol option is considered to be 326 MUS\$/million tonne (Mt) dry sugarcane biomass (bagasse and trash), including 13 MUS\$ for pentose bio-digestion in the 2 Mt capacity plant. Bonomi (2012) has presented the costs as 326 US\$/t-dry bagasse [55].

export. Notice that the study ignores the export of ethanol outside the EU and production of sugarcane bioenergy outside the Sao Paulo region in Brazil. Additionally, the study considers only two advanced conversion technologies i.e. efficient cogeneration plant and biochemical pathway via enzymatic hydrolysis. The techno-economic performance of the production of commercial bioenergy from the thermochemical route (i.e. pyrolysis/gasification) has not been considered in the analysis.

3.2. Data sources

3.2.1. Systems costs

The supply chain costs for producing energy products in the sugarcane biorefinery are divided into two categories: (a) mass or volume based fixed costs (i.e. feedstock cost, investment and operation costs) which depend upon the amount of feedstock processed and the type of conversion technologies, and (b) distance-dependent feedstock and biofuel transport costs which are determined by the mode of transport and distance traveled.

The investment costs for the conventional and upgraded technologies are presented in Table 3. Note that the costs for the juice ethanol (1G) production are the same for all technologies. The capacity of each base plant is 2 Mt sugarcane processed per year (see Table 1). The size of existing sugarcane mills in the state of Sao Paulo varies between 0.1 and 8 Mt cane per year [4] and the average output of the mills was 2 Mt of cane crushed per year in the year 2010–2011 [51]. The costs of biomass conversion technologies have scaling effects [52]. Thus, in order to incorporate or adjust the investment costs of equipment depending upon the size of sugarcane biorefinery, a scaling factor (R) is used, which is expressed as:

$$\frac{Cost_a}{Cost_{base}} = \left(\frac{Size_a}{Size_{base}} \right)^R \quad (2)$$

where $Cost_a$ and $Size_a$ represent the costs and capacity (Mt cane/year) of the equipment of the new plant respectively while $Cost_{base}$ is the known investment costs of $Size_{base}$. Considering the value of R as 0.7, the investment costs for different biorefinery sizes can be determined [53,54].

Further, investment costs of plants are annualized considering 25 years economic lifetime for the plant and an interest rate of 10% using Equation (3).

$$AC = \frac{IR}{1 - 1/(1 + IR)^t} \cdot TIC \quad (3)$$

where AC is the annualized cost, IR is the interest rate, TIC is the total investment costs, and t is the economic lifetime.

The annualized costs and operation & maintenance costs such as

spare parts, enzyme costs are summarized in Table 4. It should be noted that operation and maintenance costs increase or decrease proportionately while investment costs are adjusted exponentially as the size of the biorefining options varies. The conversion efficiencies are assumed to be constant for all sizes of biorefineries. Fig. 6 shows the costs and production efficiencies of biorefineries estimated per Mt cane plant capacity. In order to see the effect of investment and operation costs (especially enzyme cost in the 2G ethanol option), a sensitivity analysis is performed.

Fixed costs for the feedstock and distance-dependent costs for the feedstock and biofuel transport are presented in Table 5. The average cost of sugarcane is 25 US\$/t cane and the cost of trash is 15 US\$/t-dry. The total costs of trash include: windowing, baling, bale loading, trailer towing, bale transportation and bale uploading [5]. Here, the cost of bale transportation is separately considered as distance-dependent. Costs are estimated for the year 2010 considering the inflation rate in Brazil. As currency conversion between the US dollar (US\$) and Brazilian Real dollar (R\$) has significantly varied, in a range of 1.5–2.9 (US\$: R\$), during the last ten years, we consider the average conversion factor of the selected database year, including the year 2010.

In Brazil, the sugarcane is priced according to its Total Recoverable Sugar (TRS). The expression is: sugarcane price (R\$/t) = TRS price (R\$/kg of TRS) × Sugarcane quality (kg of TRS/t of sugarcane). The price of TRS is determined both by sugarcane producers and buyers based on the cost of production of sugarcane as well as the prices of ethanol and sugar, aiming at equitable distribution of profits among the producers and buyers [4].

A network map of roads is used to estimate transportation routes and distance between the sugarcane farms and biorefinery plants, as well as between biorefineries and demand areas in Sao Paulo. Distribution of biofuel outside the state of Sao Paulo is not

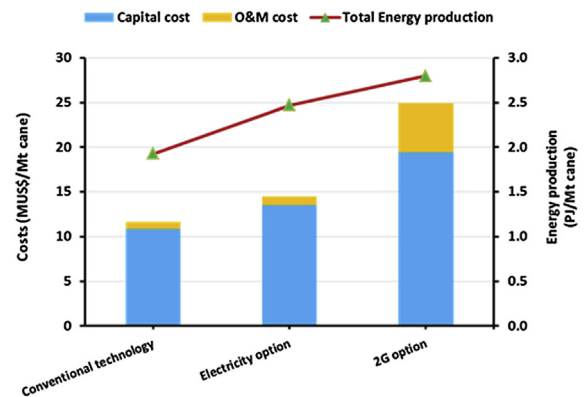


Fig. 6. Production costs and energy production per million tonne (Mt) cane.

Table 4
Annualized investment and O&M costs of biorefineries (MUSS).

Items	Technological options		
	Conventional technology	Upgraded	
		Electricity option	2G ethanol option
Annualized investment	17.7	21.9	31.5
Working capital, @5%	0.9	1.1	1.6
Start-up costs, @3%	0.5	0.7	0.9
Spare parts, @1%	0.2	0.2	0.3
Cost of enzyme (for 2G)	–	–	8.2

Notes: processing capacity considered is 2 million tonnes (Mt) per year.

Working capital, start-up, and spare part costs of the present and upgraded technologies are considered to be 5%, 3%, and 1% respectively of the annualized investment costs. Enzyme price for 2G ethanol option is assumed to be 0.1 US\$/L of 2G ethanol.

Table 5
Fixed and distance-dependent costs of feedstock and biofuel.

Parameter	Values	Units
Costs of feedstock		
Cost of sugarcane ^a	25	US\$/t cane
Cost of bagasse ^b	0	US\$/t _{dry}
Cost of trash ^c	15	US\$/t _{dry}
Costs of feedstock transport		
Sugarcane transport cost ^d	0.32	US\$/t-km
Trash transport cost ^e	0.35	US\$/t _{dry} -km
Costs of biofuel transport		
Truck ^f	5.56	US\$/km-TJ
Ocean tanker ^g	0.49	US\$/km-TJ

^a Sugarcane final price for the harvest year (2009/10) is considered which is 46.36 (R\$/t cane) i.e. 25 (US\$/t cane). See Ref. [4].

^b The cost of bagasse is considered to be zero since it is an industrial residue that is already available free at suitable conditions in sugarcane mills [26].

^c Trash biomass cost is taken from Ref. [5]. The initial US\$ value (for the year 2004) is converted into R\$, and inflation rate is applied. Finally, the cost is presented in US\$ for the year 2010. Average exchange rate for the particular year is considered.

^d The cost of sugarcane transport from field to refinery is R\$6.7 per t cane and an average distance from the farm to the mill is 22 km [56]. We consider the two-way transport.

^e Trash transport cost is taken from Ref. [5] and adjusted for the year 2010, considering the inflation rate and the average currency conversion factor. Note that the amount of trash collected/transported is only 7% (dry mass) per t cane.

^f The cost of ethanol transport from the refinery to the port by truck is R\$ 49 per m³ and average transportation distance is 499 km in 2006 [56]. The cost in US\$/km-TJ (in 2010) is estimated considering the inflation rate, average conversion factor, and two-way travel.

^g Ethanol is transported by ocean tankers from the port in Sao Paulo/Brazil to the port of Rotterdam in EU. The cost of ethanol transport by the ocean tanker is given by Ref. [56], i.e. R\$ 103 per m³. Our cost estimate is 0.49 US\$/km-TJ, considering the inflation rate and round-trip travel.

considered. In this study, heavy-duty diesel trucks are used for the transportation of feedstock (sugarcane and trash). Bioethanol within Brazil is also transported using the same diesel trucks while the export of ethanol is done by means of ocean tankers. Note that ethanol pipelines as an alternative transportation mode are not considered.

3.2.2. Lifecycle GHG emissions

In this analysis, lifecycle GHG emissions in the biofuel supply chain are evaluated. The main GHGs considered are: carbon dioxide (CO₂), methane (CH₄), and nitrous oxide (N₂O), which are converted to CO₂ equivalent (i.e.CO_{2eq}) by using Global Warming

Table 6
GHG emissions in feedstock production and processing (kgCO_{2eq}/t cane) in Brazil.

Particulars	Conventional technology	Electricity option	2G ethanol option
Feedstock production	34.7	32.1	32.1
Sugarcane farming ^a	11.7	11.7	11.7
Agricultural inputs production ^a	6.5	6.5	6.5
Trash burning ^b	—	—	—
Field emissions ^c	16.5	13.9	13.9
Feedstock processing ^d	5.6	7.5	7.8
Total emissions	40.3	39.6	39.9

^a GHG emissions from sugarcane farming and agriculture inputs production are 6.8 gCO_{2eq}/MJ and 3.8 gCO_{2eq}/MJ (anhydrous ethanol) respectively, i.e., 11.7 kgCO_{2eq}/t cane and 6.5 kgCO_{2eq}/t cane, considering ethanol yield as 81.1 L/t cane [59].

^b Trash burning practices are assumed to be eliminated.

^c Field emissions represent emissions from the soil due to fertilizers, industrial residues (returned to the soil), and limestone application. Total unburnt trash (dry kg/t cane) is 140 (conventional technology) and 70 (upgraded technologies). Nitrogen (N)-content in trash is assumed to be 0.6% (840 g/t cane for the conventional technology, and 420 g/t cane for upgraded technologies), N-input is 777 g/t cane [59]. N-content for industrial residues is: 205 g/t cane (stillage), and 264 g/t cane (filter-cake). We consider 1.325% of N in residue is converted to N in N₂O [60]. Lime application rate is 5183 g/t cane. Therefore, estimated emissions from residues is 8.1 kgCO_{2eq}/t cane (present systems), 5.5 kgCO_{2eq}/t cane (upgraded systems), and fertilizer application: 8.3 kgCO_{2eq}/t cane (i.e. nitrogen: 6.1 kgCO_{2eq} and lime: 2.3 kgCO_{2eq}/t cane).

^d Emissions (CH₄ and N₂O only) of sugarcane bagasse combustion for stationary applications is taken from GREET model [60], which is 0.0265 kgCO_{2eq}/t dry bagasse. Emissions from trash/waste and lignin combustion are considered the same as the bagasse combustion. 65% of the sugarcane biomass (bagasse and trash) is available for the electricity or 2G ethanol option. Note that emissions from biomass combustion in the 2G ethanol option is considered to be 35% of the sugarcane biomass (bagasse and trash) plus solid residues (24% lignin) obtained from the biochemical conversion in the 2G ethanol option. Emissions from the application of chemicals (1.9 kgCO_{2eq}/t cane considering juice or 1G ethanol [61] and enzyme (3.6 kgCO_{2eq}/MJ)_{2G ethanol} [62] or 3.125 kgCO_{2eq} normalized per t cane) are also considered in the estimation.

Potential (GWP) of 1, 25 and 298, respectively [57]. Emissions from (a) feedstock production and processing, (b) transport of feedstock and biofuel, and (c) substituted fossil energy carriers are considered. The cost of emitting the total GHG emissions (i.e. CO_{2eq} tax) is internalized in the model.

We account the direct GHG emissions from the following activities: (a) sugarcane farming, (b) agriculture inputs production, (c) field emissions, (d) feedstock processing, and (f) feedstock/biofuel transportation. GHG emissions (i.e. CH₄ and N₂O) from the combustion of biomass in the biorefinery are also considered. CO₂ emissions associated with biomass combustion are not accounted for since bioenergy is carbon-neutral along the biofuel chain. Emissions from embodied energy in plant and equipment are not considered. Direct and Indirect land use change (iLUC) effects are not in the scope of the analysis either since surplus sugarcane biomass (e.g. bagasse and trash) will only be used for bioenergy production without considering the expansion of sugarcane fields. However, the inclusion of indirect land use change (iLUC) can significantly affect the lifecycle greenhouse gas (GHG) emissions when it comes to the expansion of biomass/feedstock cultivation areas [58].

GHG emissions from feedstock production (sugarcane cultivation, field emissions, etc.) and feedstock processing for energy production are given in Table 6.

GHG emissions from feedstock and biofuel transport are shown in Table 7. Round-trip travel is considered. Transportation distance of feedstock and biofuel transport within Brazil varies but it is kept constant for the biofuel export from Sao Paulo to the EU port. Emission factors for fuel combustion are taken from the GREET model [60].

Avoided GHG emissions occur due to substitution of fossil fuel (i.e. gasoline) in road transport. Bioelectricity is assumed to displace marginal electricity (i.e. natural gas power) in the national grid in Brazil, instead of average electricity (mainly hydropower). However, we perform a sensitivity analysis considering a range of electricity produced from average to carbon intensive or fossil based electricity, e.g., coal power. Note that coal power is not common in Brazil but it serves as reference for other regions. Emission factors adopted in the model are presented in Table 8. Gasoline substituted is estimated considering energy equivalence (in 1:1 energy ratio) between gasoline and bioethanol, meaning that each GJ of biofuel substitutes 83.8 kg of CO_{2eq}, taking the lifecycle emission factor of gasoline from the EU's Renewable

Table 7
Emissions from feedstock and biofuel transport.^a

Parameter ^b	Values	Units
Emissions from feedstock transport ^c	112.2	tCO _{2eq} /Mt-km
Emissions from biofuel transport (Truck) ^d	5.18	tCO _{2eq} /km-PJ
Emissions from biofuel transport (Ocean tanker) ^e	0.14	tCO _{2eq} /km-PJ

^a Round-trip travel is considered. We consider road transportation using heavy-duty trucks.

^b Emission factors (grams per MJ of fuel burned) of fuel combustion (feedstock and fuel transportation) are considered from GREET model [60], i.e. 86.2 gCO_{2eq}/MJ (for heavy duty truck) and 85.8 gCO_{2eq}/MJ (for diesel ocean tanker). Energy content of ethanol (LHV) is 26.8 (MJ/kg).

^c One-way transportation distance and truck efficiency for sugarcane transport are considered as 21 km and 55 t km/L, respectively [61].

^d Emissions from ethanol transport (road) is 3.4 kgCO_{2eq}/t cane, a total transportation distance is assumed to be 340 km [61]. Emissions from the trash transport are considered to be the same as that of sugarcane transport. Note that amount of trash transported is 70 kg-dry per t cane.

^e The value of energy intensity is 0.02 MJ/t-km in the ocean tanker transport [64].

Table 8Emission factors for fossil fuel based energy (kgCO_{2q}/GJ).

Gasoline ^a	83.8
Electricity ^b	
Electricity (natural gas)	160
Electricity (Coal)	280

^a EU's Renewable Energy directive [63]. It is considered that emissions factor for gasoline is the same in Brazil and the EU.

^b Marginal electricity in Brazil is considered to be natural gas power [59]. Sensitivity analysis is performed in a range of 70 kgCO_{2eq}/GJ (average) to 280 kgCO_{2eq}/GJ (Coal). Note that Seabra and Macedo (2011) use a range of electricity emission factor from 400 to 1000 kgCO_{2eq}/MWh (i.e. about 110–280 kgCO_{2eq}/GJ) for analyzing avoided emissions [6].

Energy Directive 2009/28/EC [63].

3.2.3. Energy prices and fuel demand

a. Energy prices:

Prices for energy in transport and electricity markets highly affect the suitability of sugarcane energy products. Prices have fluctuated drastically in the last few years, especially for fossil based energy [65]. Table 9 presents the energy prices of transport fuel in Brazil and the EU, and electricity in Brazil in 2010. These are the retail prices. Note that the model considers the price of pure gasoline which is supposed to be substituted by the use of anhydrous ethanol. Sensitivity analysis is performed to include a wide range of price variation in the European and Brazilian markets.

b. Demand of biofuel and bioelectricity

The share of ethanol in the Otto-cycle vehicle was 55% in the state of Sao Paulo and 40% in Brazil as a whole in 2010. The projected amount of bioethanol consumption in Brazil is 64.6 billion liters (i.e. 1370 PJ y⁻¹), resulting in a 66% share by 2020 [67]. The internal demand of bioethanol in Brazil can be approximately met by first generation ethanol when the sugarcane production is just doubled, which is likely to happen, according to [4]. In fact, sugarcane production has grown at an average rate of 10.5% rate per year since 2000 (till 2009/10) in Brazil.

Meanwhile, the government of Brazil is making efforts to increase production of bioelectricity from sugarcane biomass (bagasse and trash). With the use of efficient cogeneration plants, sugarcane mills can provide 20% of the total electricity production

Table 9
Reference prices of transport fuel and electricity^a.

Parameters	Values	Units
Gasoline price (gasoline A) in Brazil ^b	50	US\$/GJ
Gasoline price (95 RON) in the EU ^c	65	US\$/GJ
Electricity price in Brazil ^d	55	US\$/GJ

^a Retail prices are considered for both gasoline and electricity in Brazil and the EU. The retail price of electricity represents the actual price of end-use electricity service in Brazil whereas auction prices, which are lower than the retail prices only indicate the gate prices. In the study, the retail prices are used for the modeling purpose. Sensitivity analysis is also performed taking into account a range of the prices.

^b Pure gasoline (or Gasoline A) is not sold at the gas station in Brazil. Instead, gasoline C, which is the blend of 25% anhydrous ethanol and 75% gasoline A) by volume, is used. Thus, the price of Gasoline A is estimated by the formula: "(Gasoline C price – (0.25 × Anhydrous ethanol price))/0.75". Note that the average retail prices of gasoline C and anhydrous fuel ethanol in 2010 were 2.46 and 1.52 R\$/L, respectively. Prices of gasoline C and anhydrous ethanol are obtained from Ref. [4]. Gasoline A price is expressed in US\$/GJ. Energy value (LHV) for the pure gasoline is 32.2 MJ/L.

^c Average price of unleaded petrol (95 RON) in the EU is considered to be 1.5 €/L.

^d Electricity retail price in the residential sector is considered, which is assumed to 370 R\$/MWh (i.e. 55 US\$/GJ) for the year 2009/10. Note that the regulatory agency, the Brazilian Electricity Regulatory Agency (Portuguese acronym: ANEEL), fixes the electricity tariff considering the economic/financial balance in each concession area (i.e. covering operating costs and adequate return on the capital invested), see Ref. [66].

in Brazil [21]. As mentioned earlier, in order to diversify energy products derived from the residual biomass in sugarcane bio-refineries, the production of second generation (2G) ethanol is also being promoted but still in the phase of development.

In the EU, as part of the Renewable Energy Directive (2009/28/EC), a minimum target share of 10% renewables (mainly biofuel) should be reached in the transport sector by 2020 [63]. Previously, a target of 5.75% by 2010 was set by the EU for the share of biofuels in petrol and diesel [68], but the percentage of total biofuel use in the EU member states (EU-27) only reached 4.7% in 2010 [69]. The consumption of biofuel in the EU-27 was 558 PJ y⁻¹, consisting of 21% bioethanol and 79% biodiesel in 2010. To meet the target of 10% by 2020, 1461 PJ y⁻¹ biofuel is required [68]. Second generation bioethanol from sugarcane biomass in Brazil can contribute towards this goal.

3.3. Scenarios and sensitivity analysis for upgraded technological options

We developed different scenarios for the two upgraded technological options: bioelectricity and 2G ethanol. The influencing model parameters are identified and further scrutinized. Investment and operation costs of 2G ethanol option are high compared to the electricity option. The investment cost and enzyme cost are, therefore, worth closer examination. The study examines the effect of the costs of emitting GHG emissions (i.e. carbon tax), biofuel policy support (such as tax reduction and green certificates), plant efficiencies, and the price or cost of energy services.

Table 10 shows the details of all scenarios developed. Each scenario is explicitly described. Scenario-0 is the base or reference case that reflects the existing technological and market conditions, including current costs and prices as described in data inputs (Section 3.2). Bioelectricity produced in the biorefinery displaces natural gas power, which is the main contributor of the marginal electricity generation in Brazil [59].

The model is run and sensitivity analysis is performed, taking a range of input parameters. Parameters are incrementally varied in order to see their impact. The impacts of integrated or combined parameters are also dealt with. Biofuel support is applied separately in Brazil and in the EU. Higher gasoline price in the EU

Table 10
Development of scenarios and sensitivity analysis for sugarcane biorefineries in Brazil.

Scenarios ^{a,b}	Electricity price US\$/GJ	Power plant efficiency improvement (%)	Emission factor (electricity) kgCO _{2eq} /GJ	Investment cost (2G) ^c (%)	Enzyme cost (2G) (%)	Gasoline price		Biofuel support		Carbon tax US\$/tCO _{2eq}	Scenario description
						EU	Brazil	EU	Brazil		
						US\$/GJ	US\$/GJ	US\$/GJ	US\$/GJ		
Sc-0	55	–	0.16	–	–	65	50	0	0	50	Reference or base case with existing conditions (e.g. efficiencies, natural gas power as marginal electricity), current costs and prices, carbon tax: 50 US\$/tCO _{2eq} , and no biofuel support.
Sc-1	(55–80)	–	0.16	–	–	65	50	0	0	50	Electricity price varies between 55 and 80 US\$/GJ.
Sc-2	(80)	–	0.16	–	–	65	50	(3–10)	0	50	Electricity price is set at 80 US\$/GJ in Brazil, but biofuel support (US\$/GJ) applied in the EU.
Sc-3	55	–	0.16	(15–90)	–	65	50	0	0	50	Total Investment cost of 2G ethanol option is increased up to 90% while investments for the current technology and electricity option are kept constant.
Sc-4	55	–	0.16	–	(150–400)	65	50	0	0	50	Operation cost (i.e. cost of enzyme) for 2G ethanol option is increased - up from 150% to 400%.
Sc-5	55	–	0.16	(100)	–	65	50	(1–40)	0	50	Investment cost of 2G ethanol option is increased by two-fold but there exists biofuel support in the EU.
Sc-6	55	–	(0.28)	–	–	65	50	0	0	(70–150)	Fossil based electricity (emission factor: 0.28 kgCO _{2eq} /MJ) is considered as marginal electricity in Brazil. Options are simulated at the varying carbon tax rates (US\$/tCO _{2eq}).
Sc-7	55	(0–35)	0.16	–	–	65	50	0	0	50	Power plant efficiency is increased up to 35%.
Sc-8	55	(50)	0.16	–	–	65	50	(6–15)	0	50	Improved efficiency in power conversion is set at 50% while biofuel support (US\$/GJ) is provided in the EU.
Sc-9	(50–61)	–	0.16	–	–	(low, <50)	50	0	0	50	Price of fossil fuel is kept low (<50 US\$/GJ) in the EU, there will be no export of 2G ethanol, making conflict between 2G ethanol and bioelectricity within Brazil at the varying price of electricity.
Sc-10	(65)	–	0.16	–	–	(low, <50)	50	0	(1–10)	50	Gasoline price in the EU is kept less than 50 US\$/GJ, electricity price in Brazil is set at 65 US\$/GJ while biofuel support for 2G ethanol option, in a range of 1–10 US\$/GJ, is applied in Brazil.
Sc-11	55	–	0.16	(0–25)	–	(low, <50)	50	0	0	50	Gasoline price in the EU is kept less than 50 US\$/GJ, total investment cost of 2G ethanol option is increased up to 25%, keeping investments for reference technology and electricity option at the reference level.
Sc-12	55	(50)	0.16	–	–	(low, <50)	50	0	(15–25)	50	Gasoline price in the EU is kept less than 50 US\$/GJ, power plant efficiency is increased up to 50% while biofuel support is applied in Brazil.
Sc-13	55	–	(0.09–0.28)	–	–	(low, <50)	50	0	0	50	Gasoline price in the EU is kept less than 50 US\$/GJ, emission factor for substituted or displaced electricity is varied from 0.09 to 0.28 kgCO _{2eq} /MJ.
Sc-14	55	–	0.16	–	–	(low, <50)	50	0	0	(75–275)	Gasoline price in the EU is kept less than 50 US\$/GJ, natural gas power (emission factor: 0.16 kgCO _{2eq} /MJ) is considered as marginal electricity in Brazil, options are simulated at the varying carbon tax rates (US\$/tCO _{2eq}).

^a Scenarios 1–8 consider the current gasoline prices in the EU and Brazil.

^b Scenarios 9–14 study the conflict between 2G ethanol and bioelectricity within Brazil, setting an unfavorable condition for ethanol export to the EU.

^c Investment costs refer to the total set-up costs (including upgraded systems costs) of the individual biorefinery.

Table 11
Categorization of parameters and scenarios.

Parameter categories	Scenarios ^a	
	Current price of gasoline in the EU (export to the EU) ^b	Reduced price of gasoline in the EU (no export to the EU) ^c
a. Market and technological impacts		
Market price of fuel/energy	Sc-1	Sc-9
Type of substituted power	–	Sc-13
Investment and operation costs	Sc-3, Sc-4	Sc-11
Plant efficiency	Sc-7	–
b. Policy impacts		
Biofuel support	Sc-2, Sc-5, Sc-8	Sc-10, Sc-12
Carbon tax	Sc-6	Sc-14

Notes:

^a See Table 10 for details about scenarios.

^b The price of fossil fuel in the EU is US\$65/GJ, as in the case of reference case.

^c The price of fossil fuel in the EU is low (i.e. less than 50 US\$/GJ), that does not allow exporting 2G ethanol.

noticeably favors the export of the 2G ethanol from Brazil. Scenarios 1–8 examine the optimal choice between producing 2G ethanol and exporting to the EU and bioelectricity in Brazil. However, lower price of gasoline in the EU allows the use of 2G ethanol in Brazil, depending upon its competitiveness against bioelectricity. Scenarios 9–14 consider the analysis of 2G ethanol and/or bioelectricity option in Brazil.

4. Results and discussions

The study shows that it is worthwhile to upgrade sugarcane biorefineries for the production of more energy services in the form of second generation (2G) ethanol and/or bioelectricity using residual sugarcane biomass. We discuss here the results obtained from the scenario analysis, particularly focusing on the factors that most influence the technological options.

4.1. Reference scenario

In the base or reference scenario Sc-0, in which present conditions apply, it is optimal to produce 2G ethanol in Brazil and export to the EU. Total 1G and 2G ethanol production is 668 PJ y⁻¹ and 301 PJ y⁻¹, respectively. The total lifecycle GHG emissions are estimated to be 16.8 Mt.CO_{2eq}y⁻¹. The result indicates that 2G ethanol could amount to 2.5% of the EU transport fuel consumption in 2010, which is a significant share of contribution to the EU transport fuel mix. Fig. 7 shows the share of emissions and costs along the biofuel chain. Emissions from feedstock production correspond to the largest share of emissions along the fuel chain i.e. 66%, followed by plant emissions (16%), and feedstock transport (11%). When it comes to costs feedstock cost contributes only 37% (see Fig. 7). The use of ethanol in transport will substitute gasoline and subsequently remove 55 Mt.CO_{2eq} in Brazil and 25 Mt.CO_{2eq} in the EU, thus resulting in 79.4% total emissions savings compared to conventional fossil fuel. The total cost of producing ethanol (1G and 2G) is US\$24.9/GJ. The value is comparable to the cost of producing first generation (1G) ethanol in the US and Brazil. Note that the cost of corn ethanol production in the US (net of co-product credit) was US\$19.3/GJ and sugarcane juice ethanol in Brazil was US\$18.7–32.6/GJ in a range of 1.55–2.62 (US\$: R\$) currency conversion [56].

4.2. Determining the impact of key parameters: scenario and sensitivity analysis

The study finds that the main parameters influencing the choice of technological options are: electricity price, set-up and operation

costs, type of marginal electricity substituted, power plant efficiency, gasoline price, and policy instruments (i.e. biofuel support and carbon tax). Results are obtained by varying individual parameters. It should be noted that a few scenarios (i.e. Sc 9–14) are also developed to study the choice of bioelectricity and/or 2G ethanol options within Brazil, limiting the export of 2G ethanol in the EU (see Table 10, Section 3.3). However, it is rather difficult to directly compare the results with the existing techno-economic optimization studies at the plant level in Brazil due to its scope of the study/systems boundary, inclusion of all biorefineries in the state of Sao Paulo, and policy impacts. Results of different scenarios are broadly divided into two categories: (a) technological and market impacts, viz., plant efficiency, investment and operation costs, type of substituted power, and market price of fuel/energy, and (b) policy impacts, i.e. biofuel support and carbon tax. Table 11 summarizes the impacts analyzed in the study, considering the parameter categories and conditions for exports or no exports of 2G ethanol to the EU.

4.2.1. Influence of market and technological factors on the technological choice

The impact of electricity price in Brazil is scrutinized in scenarios Sc-1 and Sc-9 with the base case and at the low fossil fuel price in the EU, respectively. Fig. 8(a) shows that the 2G ethanol option is left in favor of the electricity option when the price of electricity goes from 68 US\$/GJ in the base case to 76 US\$/GJ. At 72 US\$/GJ price, 41% of all sugarcane biorefineries select the electricity option and the others remain in the 2G ethanol option. The corresponding amount of energy products are 54 PJ bioelectricity (20% share) and 214 PJ second generation (2G) ethanol. Note that all plants would be converted into the bioelectricity production option at an electricity price of 76 US\$/GJ, which is 38% higher than the base case price.

Scenario Sc-9 considers the effect of the electricity price when the export of 2G ethanol is limited, by setting fossil fuel price low at 50 US\$/GJ in the EU, which makes the suitability analysis between 2G ethanol and electricity production in the energy systems in Brazil. The majority of biorefineries would opt for the electricity option when the price of electricity exceeds 60 US\$/GJ. Thus, if the system does not allow 2G ethanol exports, there is no strong support for producing 2G ethanol. A small increase (i.e. 9%) in the electricity price is enough to motivate the electricity option, see Fig. 8(b). It is also verified that energy market prices of 2G ethanol and bioelectricity play a key role in determining economic performances of a flexible sugarcane biorefinery [30,31].

In the reference scenario (Sc-0), marginal electricity in Brazil is natural gas power (electricity emission factor: 0.16 kgCO_{2eq}/MJ).

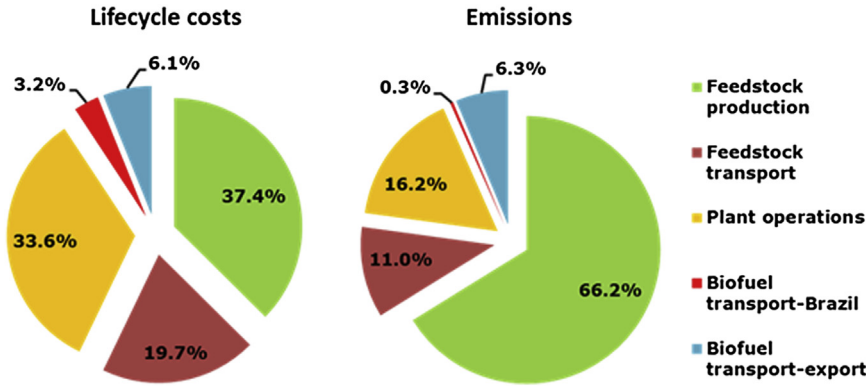


Fig. 7. Lifecycle costs (left) and emissions (right) along the biofuel supply chain (scenario Sc-0).

Even if the marginal electricity were carbon-intensive coal power (electricity emission factor: 0.28 kgCO_{2eq}/MJ), it is optimal to produce 2G ethanol for export to the EU (Scenario Sc-6 at the base case 50 US\$/tCO_{2eq} carbon tax). In contrast, with the case of no export of 2G ethanol to the EU (scenario Sc-13), electricity emissions factor i.e. type of marginal or substituted electricity would determine the choice of ethanol and/or electricity configuration (see Fig. 9). For example, high electricity emission factor 0.28 kgCO_{2eq}/MJ favors the production of electricity optimally.

The production of 2G ethanol is still in the phase of research and development. Therefore, it is likely that the investment and operation costs would increase in the future. The effect of increase in the 2G ethanol set-up cost and enzyme costs are performed in scenarios Sc-3, Sc-4 and Sc-11, keeping the investment costs of bioelectricity technology constant. Operation cost (mainly enzyme cost) does not have a high impact until its 3-fold increase at the reference condition. Furlan et al. (2013) also found that the impact of enzyme cost on the Internal Rate of Return (IRR) of a flexible sugarcane biorefinery was not significant [31]. However, investment costs have a significant role in determining the technological options with or without ethanol exports to the EU, see Fig. 10. For example, a 75% increase in the cost of the 2G option would convert 84% of sugarcane biorefineries into the electricity option if we consider the export of ethanol, see Fig. 10a. It is more sensitive with the condition of no export since 25% increase in the investment cost would prompt to select the electricity option (Fig. 10b). Of the total, 108 biorefineries will select the electricity option if the investment cost of 2G option increases 20%.

In the reference scenario Sc-0, power plant efficiency is set at 150 kWh/t cane (i.e. 1.93 PJ/Mt cane). The technology considered is

condensing-cum-extraction steam turbine (CEST). With the use of biomass integrated gasification combined cycle (BIG-CC) technology, electrical efficiency can be increased to more than 250 kW/t cane (Khatiwada et al., 2012). In scenario Sc-7, the impact of plant efficiency is analyzed. The study finds that if conversion efficiency is increased by 35% (i.e. 202.5 kWh/t cane), all plants are selected to produce electricity optimally, see Fig. 11. However, biofuel support (i.e. incentives or subsidies) of 15 US\$/GJ in the EU can create a shift towards the 2G option even if the conversion efficiency is doubled (Scenario Sc-8)

The study also reveals that the number of ethanol and/or electricity options selected and corresponding energy production are

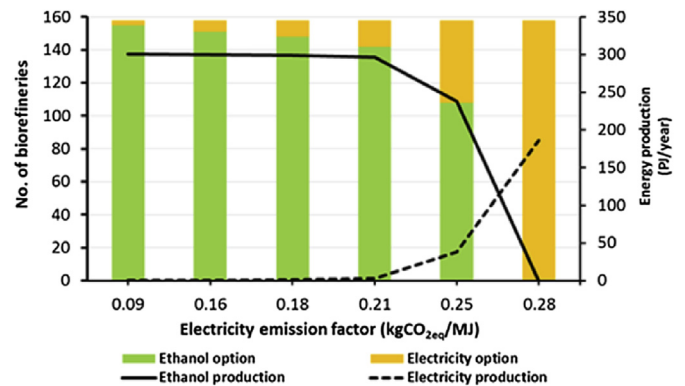
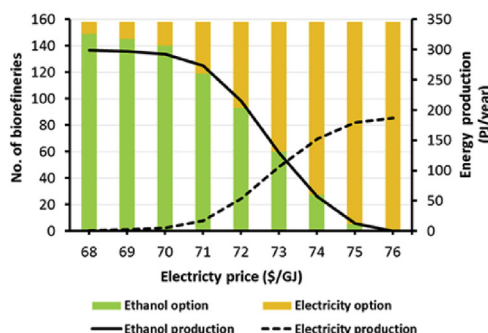


Fig. 9. Impact of the type of substituted electricity (Sc-13) (expressed in electricity emission factor) base case with no export of ethanol (i.e. low fossil fuel price in the EU).

a. At the base case (Sc-1)



b. At the low fossil fuel price (<50 US\$/GJ) in the EU (Sc-9)

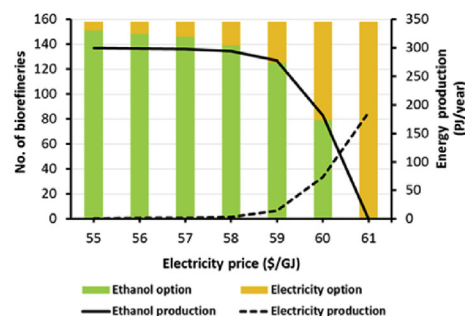


Fig. 8. Impact of the electricity price at the base case and low fossil fuel price conditions (Sc-1 and Sc-9).

not proportionally related in all scenarios, mainly because of economies of scale. Biomass conversion technologies considered in this study, viz., condensing-cum-extraction steam turbine (CEST) based cogeneration plant for electricity option and biochemical conversion for second generation (2G) ethanol option are at different level of technological and commercial development. CEST is commercially available whereas 2G option is still in the phase of development. Therefore, it is important to simulate model results, considering technological improvements in terms of systems costs and conversion efficiency.

4.2.2. Influence of policy on the technological choice

The impacts of biofuel support and carbon tax policy instruments in both EU and Brazil are evaluated in various scenarios (see Table 11). As discussed earlier, when the price of electricity increases above 76 US\$/GJ, the model selects the electricity option (scenario Sc-1). However, biofuel support applied in the EU has the potential to make the 2G option optimally feasible (scenario Sc-2). Fig. 12(a) shows the extent to which biofuel support in the EU promotes 2G ethanol in Brazil. For instance, 5 US\$/GJ support help converting more than 60% of biorefineries into 2G ethanol option even if the electricity price is quite high in Brazil. On the other hand, when the investment cost of 2G option increases by two-fold (scenario Sc-5), 5 US\$/GJ biofuel support will only motivate the conversion of 23% of the biorefineries into the 2G option, resulting in 96 PJ of ethanol exports to the EU, see Fig. 12(b).

When looking at the impact of biofuel support in Brazil (without ethanol export) at an elevated electricity price of 65 US\$/GJ (scenario Sc-10), 3–5 US\$/GJ support in terms of incentive/subsidies or green certificate would convert more than 90% of biorefineries into 2G ethanol option. However, 16.5 US\$/GJ biofuel support can only convert 51% of the biorefineries for the production of 2G ethanol when 50% more efficient power plant is considered (scenario Sc-12).

At the moment, Brazil does not have carbon pricing scheme. Therefore, results on the impacts of carbon tax are indicative and it may not be directly applied in the present context. But it is evident that the policy support such as carbon tax is an efficient economic instrument to mitigation GHG emissions and it could significantly help to promote renewable energy using the carbon tax revenue [70,71]. The illustration helps provide a clear indication on the impacts of carbon tax for the production of bioelectricity and/or 2G ethanol in sugarcane biorefineries. The study finds that carbon tax does not have a significant impact when natural gas power is considered as marginal electricity in Brazil. But, if carbon intensive fossil based electricity (e.g. coal power) is considered as marginal

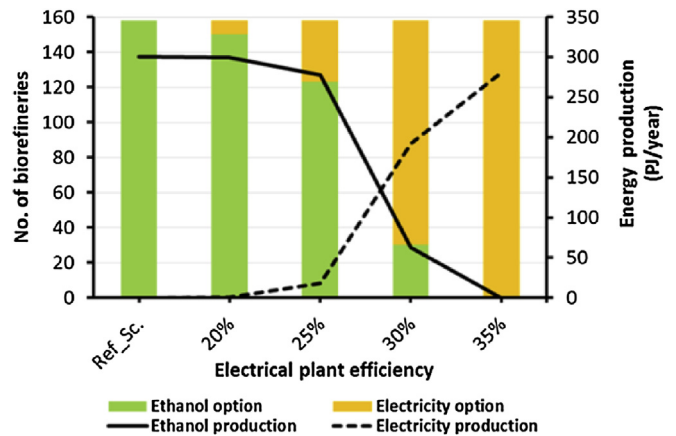


Fig. 11. Impact of power plant efficiency.

electricity (scenario Sc-6), carbon tax can play a key role in shifting 2G ethanol towards the electricity option as seen in Fig. 13. The study finds, in this case, that all plants would be converted into electricity option at a carbon tax of US\$ 150 tCO_{2eq}. Although coal-fired power plants correspond to only 1.7% of the total installed capacity in Brazil [72], it is worth keeping in mind for the case of other countries.

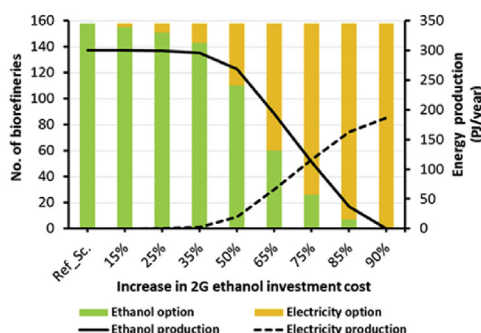
It is important to mention that a carbon tax (US\$/tCO_{2eq}) is directly linked to the level of carbon dioxide equivalent (CO_{2eq}) emissions. As part of energy sector reform and climate change mitigation actions, a few developed and developing countries have already introduced the carbon taxes [73]. For example, Sweden has introduced a carbon tax in 1991 and the value is US\$ 168 per tCO_{2eq} in 2014 [73]. Therefore, the inclusion of the carbon tax as a new regime for carbon compensation could play a vital role for substituting carbon-intensive fossil based electricity and promoting international biofuel trade in the EU.

Similarly, at a reduced gasoline price in the EU and thus without 2G ethanol export (scenario Sc-14), carbon tax will have an impact on the selection of technological options. For example, 60% of plants shift towards the electricity option when US\$ 250 tCO_{2eq} carbon tax is applied. It should be noted that marginal electricity for this scenario is natural gas power.

5. Conclusions

In Brazil, sugar and ethanol mills can be upgraded for

a. With condition of ethanol export to the EU (Sc-3)



b. Without condition of export (i.e., at the low gasoline price: <50 \$/GJ) in the EU (Sc-11)

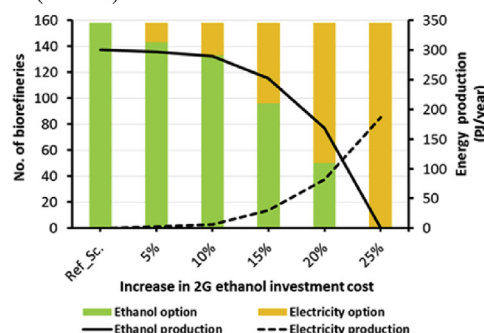


Fig. 10. Impacts of 2G ethanol investment costs (Sc-3 and Sc-11).

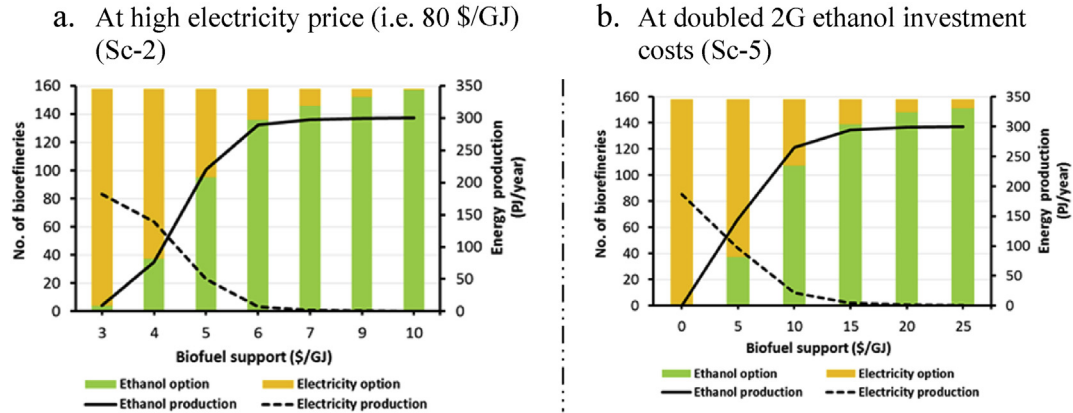


Fig. 12. Biofuel support when electricity price and investment costs are high.

bioelectricity and/or second generation (2G) bioethanol using residual sugarcane biomass (bagasse and trash). This study has investigated two technological pathways for improving the energy production capacity of existing sugarcane mills. Efficient cogeneration for bioelectricity and biochemical conversion technology for 2G ethanol are considered. All sugarcane mills located in the state of Sao Paulo in Brazil are included in the simulation.

The study performs a techno-economic analysis of the improved sugarcane biorefineries considering a spatially explicit optimization model for minimizing the system costs in the entire fuel chain. Carbon costs are internalized in the model. Bioelectricity is provided to the grid and second generation (2G) ethanol production allows exports to the EU. The model determines which technological option is optimal, and at what point exports are justified. As the size and location of biorefineries is different, the model selects a combination of technological options with distinct spatial location. This study would definitely complement the existing research studies on the optimization of biorefineries, taking into account the entire production chains of biofuel/bioelectricity production in the region (the state of Sao Paulo), domestic biofuel demand in Brazil and trade to the EU, associated market prices, and policy instruments.

At the reference scenario, with a relatively high cost of fossil based transport fuel in the EU and natural gas derived power as marginal electricity in Brazil, the 2G ethanol option is more favorable. Produced 2G ethanol would then be exported to the EU, contributing to a share of 2.5% of the total transport fuel in the EU in

2010.

Market and technological factors such as energy prices, plant efficiency and costs, type of substituted electricity, and policy instruments such as carbon tax and biofuel support are found to be the factors that most influence the outcome. When the price of electricity exceeds 75 US\$/GJ, all sugarcane mills would shift towards the bioelectricity option. The study finds that a gasoline price below 50 US\$/GJ in the EU is not attractive to motivate exports of second generation (2G) ethanol from Brazil.

Conversion efficiency may also have a significant impact on the choice of technology. For example, if power plant efficiency is increased by 35% (i.e. 202.5 kWh/t cane), all plants are optimally selected to produce electricity. Biofuel support applied in the EU or in Brazil can promote the 2G ethanol option, even at a higher electricity price in Brazil or in the case of increased investment costs. When the investment cost of 2G ethanol option increases by two-fold, 5 \$US/GJ biofuel support is enough to convert 23% of biorefineries into the 2G option, leading to exports of 96 PJ of ethanol to the EU. The study finds that the generation of bioelectricity would be optimal when a combination of carbon-intensive electricity and a high emission tax is applied in Brazil.

This study is mainly focused on the technological upgrading of existing sugarcane mills, but it would also be important to look into the new sugarcane mills as ethanol production expands. The model can be further developed for identifying the optimum size and location of the future sugarcane biorefineries for minimization of the total system costs and carbon costs in Brazil. It can also be applied to other sugarcane producing countries since there is a great potential to utilize surplus sugarcane biomass around the world. Different configurations such as stand-alone and integrated/clustered or flexible, and conversion technologies, viz. thermochemical routes can also be simulated for finding suitable technological options, also considering both energy (power generation or biofuel production) and non-energy bioproducts.

Production of sugarcane is seasonal. There is also scope for utilizing other agricultural residues, e.g., rice husk and wheat straw, in synergy with sugarcane biorefineries for optimal production of energy services. Present studies on the performances of integrated and flexible biorefineries for the production of multiple energy and non-energy products/services should be incorporated in selecting important parameters (e.g. costs and conversion efficiencies) and their values which are the main inputs for this spatially explicit techno-economic model.

The model developed in this study could be useful in utilizing other abandoned or unutilized agricultural harvest residues and co-products/residues left over from industrial processes for energy

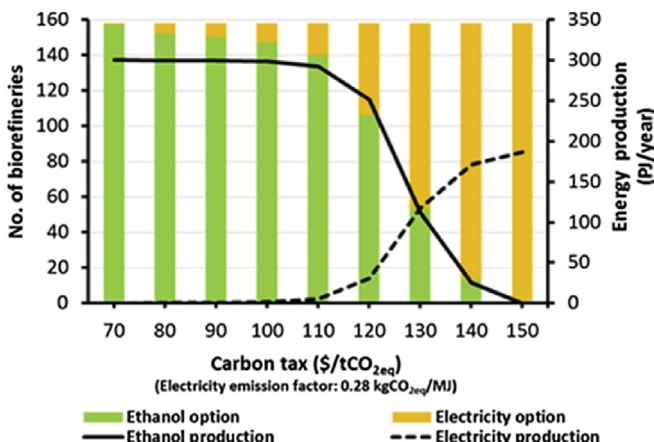


Fig. 13. Effects of carbon tax on carbon-intensive fossil based electricity (Sc-6).

production since residual feedstock does not compete with food production and land use. The paper has presented the conditions and amount of 2G ethanol to be imported in the EU from Brazil. International trade of biofuels offers win–win opportunities to Brazil and the EU when it comes to meeting the national renewable targets, enhancing competitiveness of the biofuel industries, and promoting sustainable development.

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